Amendment to Claims:

1. (currently amended): A process for producing a dried carboxylic acid cake, said process comprising:

(a) oxidizing in an oxidation zone an aromatic feedstock to produce a carboxylic acid slurry;

~~(a)~~(b) removing in a liquor exchange zone impurities from saida carboxylic acid slurry to form a water-wet carboxylic acid cake, a mother liquor stream, a solvent mother liquor stream, and a solvent/water byproduct liquor stream; wherein solvent or water is added counter current to the flow of said carboxylic acid slurry; and

~~(b)~~(c) drying said water-wet carboxylic acid cake or carboxylic acid cake with solvent in a drying zone to form said dried carboxylic acid cake.

2. (original): The process according to claim 1 wherein said liquor exchange zone comprises from about 2 to about 4 stages of water or solvent counter current washes.

3. (original): The process according to claim 1 wherein said solvent and said water is added counter current to the flow of said carboxylic acid slurry.

4. (original): A process according to claim 1 wherein said carboxylic acid is selected from a group consisting of terephthalic acid, isophthalic acid, naphthalene dicarboxylic acid, trimellitic acid, and mixtures thereof.

5. (original): A process according to claim 1 wherein said carboxylic acid is terephthalic acid.

6. (original): A process according to claim 1, 2 or 3 wherein said drying zone evaporates at least 10% of volatiles in said water-wet carboxylic acid cake.

7. (currently amended): A process according to claim 1 wherein said crude carboxylic acid slurry comprising terephthalic acid, catalyst, acetic acid, and impurities is

withdrawn at a temperature between about 110°C to about 200°C from an oxidation zone; wherein said catalyst comprises cobalt, manganese and bromine compounds.

8. (currently amended): A process for producing a dried carboxylic acid cake, said process comprising:

(a) oxidizing in an oxidation zone an aromatic feedstock to produce a carboxylic acid slurry;

~~(a)~~(b) removing in a solvent liquor exchange zone impurities from a carboxylic acid slurry to form a carboxylic acid cake with solvent, a mother liquor stream, and a solvent mother liquor stream;

~~(b)~~(c) optionally, adding water in a counter current water wash zone to said carboxylic cake with solvent to produce a water-wet carboxylic acid cake and a solvent/water by product liquor stream; and

~~(c)~~(d) drying said water-wet carboxylic acid cake or said carboxylic acid cake with solvent in a drying zone to form said dried carboxylic acid cake.

9. (original): A process according to claim 8 wherein said carboxylic acid is selected from a group consisting of terephthalic acid, isophthalic acid, naphthalene dicarboxylic acid, trimellitic acid,and mixtures thereof.

10. (original): A process according to claim 8 wherein said carboxylic acid is terephthalic acid.

11. (original): A process according to claim 8 or 9 wherein said drying zone evaporates at least 10% of volatiles in said water-wet carboxylic acid cake.

12. (currently amended): A process according to claim 8 wherein said crude carboxylic acid slurry comprising terephthalic acid, catalyst, acetic acid, and impurities is

withdrawn at a temperature between about 110°C to about 200°C from an oxidation zone; wherein said catalyst comprises cobalt, manganese and bromine compounds.

13. (currently amended): A process for producing a dried carboxylic acid cake, said process comprising:

(a) oxidizing in an oxidation zone an aromatic feedstock to produce a carboxylic acid slurry;

~~(a)~~(b) removing in a solid-liquid separation zone impurities from asaid carboxylic acid slurry to form a slurry or cake product and a mother liquor stream;

~~(b)~~(c) removing in a counter current solvent-water liquor exchange zone residual impurities from said slurry or cake product to form a water-wet carboxylic acid cake, a solvent mother liquor stream, and a solvent/water byproduct liquor stream; wherein said counter current solvent-water liquor exchange zone comprises one solid-liquid separation device; and

~~(c)~~(d) drying said water-wet carboxylic acid cake or said carboxylic acid cake with solvent in a drying zone to form said dried carboxylic acid cake.

14. (original): A process according to claim 13 wherein said carboxylic acid is selected from a group consisting of terephthalic acid, isophthalic acid, naphthalene dicarboxylic acid, trimellitic acid and mixtures thereof.

15. (original): A process according to claim 13 wherein said carboxylic acid is terephthalic acid.

16. (currently amended): A process according to claim 13 wherein said crude carboxylic acid slurry comprising terephthalic acid, catalyst, acetic acid, and impurities is withdrawn at a temperature between about 110°C to about 200°C from an oxidation

zone; and wherein said catalyst comprises cobalt, manganese and bromine compounds.

17. (original): A process according to claim 13 or 14 wherein said drying zone evaporates at least 10% of volatiles in said water-wet carboxylic acid cake.

18. (currently amended): A process for producing a dried carboxylic acid cake, said process comprising the following steps:

(a) removing a solvent from a slurry or cake product in a counter current solvent-water liquor exchange zone; wherein a ~~substantial~~ portion of the solvent in said slurry or cake product is replaced with water to form a water-wet carboxylic acid cake; wherein said counter current solvent-water liquor exchange zone comprises one solid-liquid separation device; and

(b) drying said water-wet carboxylic acid cake or said carboxylic acid cake with solvent in a drying zone to form said dried carboxylic acid cake.

19. (orginal): A process according to claim 18 wherein said carboxylic acid is selected from a group consisting of terephthalic acid, isophthalic acid, naphthalene dicarboxylic acid, trimellitic and mixtures thereof.

20. (original): A process according to claim 18 wherein said carboxylic acid is terephthalic acid.

21. (currently amended): A process according to claim 19 wherein said crude carboxylic acid slurry comprising terephthalic acid, catalyst, acetic acid, and impurities is withdrawn at a temperature between about 110°C to about 200°C from an oxidation zone; and wherein said catalyst comprises cobalt, manganese and bromine compounds.

22. (original): A process according to claim 18 or 19 wherein said drying zone evaporates at least 10% of volatiles in said water-wet carboxylic acid cake.

23-47. (canceled)